

In the Claims:

Please amend the claims as follows:

1. (Currently Amended) A process for the catalytic dewaxing of a hydrocarbon oil feed selected from the group consisting of solvent extracted waxy raffinate, gas oil and hydrocracker feedstock wherein said hydrocarbon oil feed ~~including~~ includes waxy molecules and more than ~~500~~ 1000 ppmw of sulphur or sulphur containing compounds by contacting the oil feed under catalytic dewaxing conditions with a catalyst composition ~~comprising~~ consisting essentially of a Group VIII metal hydrogenation component, dealuminated aluminosilicate zeolite crystallites and a low acidity refractory oxide binder material which is essentially free of alumina.

Cancel claim 2.

3. (Previously Amended) The process of claim 1, in which the oil feed comprises more than 10 ppmw of nitrogen or nitrogen containing compounds.

4. (Previously Amended) The process of claim 1, in which the hydrogenation component is platinum, palladium or nickel.

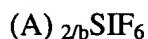
5. (Previously Amended) The process of claim 1, in which the low acidity binder is silica.

6. (Previously Amended) The process of claim 1, in which the aluminosilicate zeolite crystallites have a Constraint Index of between 2 and 12.

7. (Previousl Amended) The process of claim 6, in which the aluminosilicate zeolite crystallites include MFI type zeolite.

8. (Previously Amended) The process of claim 1, in which the dealuminated aluminosilicate zeolite crystallites are obtained by contacting the zeolite crystallites with an

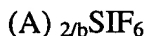
aqueous solution of a fluorosilicate salt wherein the fluorosilicate salt is represented by the formula:



in which 'A' is a metallic or non-metallic cation other than H<sup>+</sup> having the valence 'b'.

9. (Previously Amended) The process of claim 8, in which an extrudate of the aluminosilicate zeolite crystallites and the low acidity binder is contacted with the aqueous solution of the fluorosilicate salt.
10. (Previously Amended) The process of claim 1, in which the oil feed is a solvent extracted waxy raffinate.
11. (Previously Amended) The process of claim 1, in which the oil feed is a gas oil.
12. (Previously Amended) The process of claim 1, in which the oil feed is a hydrocracker feedstock and wherein the dewaxed oil is subsequently subjected to a hydrotreating step before being subjected to a hydrocracker process step in which step primarily middle distillates are prepared.
13. (Previously Amended) A method of retrofitting a process for preparing lubricating base oils in which an existing solvent dewaxing step is replaced by a catalytic dewaxing process comprising the steps of contacting the oil feed under catalytic dewaxing conditions with a catalyst composition comprising a Group VIII metal hydrogenation component, dealuminated aluminosilicate zeolite crystallites and a low acidity refractory oxide binder material which is essentially free of alumina of claim 1.
14. (Original) The process of claim 8, where 'b' is ammonium.
15. (Original) The process of claim 1, in which the hydrogenation component is palladium.

16. (Original) The process of claim 1, in which the hydrogenation component is nickel.
17. (New) A process for the catalytic dewaxing of a hydrocarbon oil feed selected from the group consisting of solvent extracted waxy raffinate, gas oil, and hydrocracker feedstock wherein said hydrocarbon oil feed includes waxy molecules and more than 1000 ppmw of sulphur or sulphur containing compounds by contacting said hydrocarbon oil feed under catalytic dewaxing conditions with a catalyst composition comprising a nickel hydrogenation component, dealuminated aluminosilicate zeolite crystallites and a low acidity refractory oxide binder material which is essentially free of alumina.
18. (New) The process of claim 17, wherein said hydrocarbon oil feed comprises more than 10 ppmw of nitrogen or nitrogen containing compounds.
19. (New) The process of claim 18, wherein said low acidity binder is silica.
20. (New) The process of claim 19, wherein said aluminosilicate zeolite crystallites have a Constraint Index of between 2 and 12.
21. (New) The process of claim 20, wherein said aluminosilicate zeolite crystallites include MFI type zeolite.
22. (New) The process of claim 21, wherein said dealuminated aluminosilicate zeolite crystallites are obtained by contacting the zeolite crystallites with an aqueous solution of a fluorosilicate salt wherein the fluorosilicate salt is represented by the formula:



in which 'A' is a metallic or non-metallic cation other than H<sup>+</sup> having the valence 'b'.

23. (New) The process of claim 22, wherein an extrudate of the aluminosilicate zeolite crystallites and the low acidity binder is contacted with the aqueous solution of the fluorosilicate salt.
24. (New) The process of claim 23, wherein 'b' is ammonium.
25. (New) The process of claim 24, wherein said catalyst composition has an absence of a Group VIB metal component.